CO, NI AND K AS PROMOTERS IN CO₂ HYDROGENATION ON M₀S₂ BASED CATALYSTS

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INTRODUCTION

 CO_2 is a well know greenhouse gas and the amount in the atmosphere is still rising. The goal of this work was to study recycling and utilization of carbon dioxide in flue gas by catalytic reduction. Flue gas contains about 10 - 15 vol.% CO_2 , oxygen, water and traces of sulfur containing substances like H₂S. There are several ways to convert CO_2 into valuable compounds using different catalysts. For example: Ni based catalysts for CH_4 formation, $Cu/ZnO/Al_2O_3$ for methanol production or MoS_2 based catalysts for alcohol synthesis. However, the sulfur contamination in the flue gas leads to deactivation of many catalysts. MoS₂ based catalysts should not be affected by sulfur containing feed gas. Co-Mo-S materials are known as hydrodesulfurization catalysts and are also active for CO_2 hydrogenation. ^[1] Therefore, in this work, we have studied MoS_2 based catalysts in order to learn about correlations between synthesis and composition, structural and catalytic properties.

EXPERIMENTS

In this work different formulations of Co-Mo-S and Ni-Mo-S catalysts were prepared hydrothermally ^{[2], [3]} and by precipitation ^[4] and compared to each other. Different supports (activated carbon and alumina) were used. Catalysts with and without potassium promoter were synthesized. Catalytic properties were tested in a plug flow reactor up to 20 bar. Reaction orders of the reactants and apparent activation energies of the product formation were calculated. A long-term test was done to ensure the stability of the catalyst.

The catalysts were characterized by TPD (temperature programmed desorption), TPR (temperature

programmed reduction), TPO (temperature programmed oxidation), XRD (X-ray diffraction) and N_2 physisorption and the changes of the catalyst during the reaction were investigated.

RESULTS AND DISCUSSION

Products were mainly CO, methane and traces of methanol. Fig. 1 shows the yield of CO and CH_4 over different Co-Mo-S catalysts. The effect of potassium as promoter was investigated. Catalysts with potassium promoter produced much less CH_4 and more CO under the given conditions. There was no dependence on the support.



Fig. 1: Yield of CO and CH₄ at 330 °C, 21 bar, 3000 mlN/($g_{catalyst}$ *h)

Fig. 2 shows the conversion of a $MoS_2 + K$ catalyst compared to a Co-Mo-S + K catalyst. The conversion of the Co-Mo-S + K catalyst was higher at the given conditions. The Co-Mo-S + K catalyst showed a lower selectivity to CH₄.

A long-term test over 200 hours showed a constant conversion of CO_2 over the catalyst.

Under reducing conditions, the catalyst was stable below 500 $^{\circ}$ C, whereas under oxidizing condition above 300 $^{\circ}$ C SO₂ was formed.

XRD showed a change of the cobalt sulfide phase during the reaction.



Fig. 2: Conversion of CO_2 over $MoS_2 + K$ and Co-Mo-S + K, 21 bar, 300 mlN/($g_{catalyst}*h$)

CONSLUSION

Co, Ni and K are efficient promoters of MoS_2 based catalysts to increase the formation of CO and inhibit the CH_4 production. The catalyst was stable under working conditions.

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